

Modelling fluid-grain interactions in two phase materials Discrete element–lattice Boltzmann coupled methods

Olek Zienkiewicz Course 2011
Discrete Mechanics of Geomaterials

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Warning!

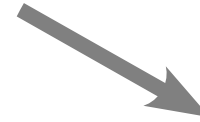
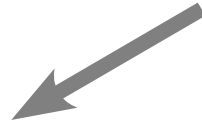
This presentation does not aim to give a state of the art about the lattice Boltzmann method and its coupling with DEM.

This presentation just gives an insight into a such approach and it is based on a development work still in progress, mistakes certainly exist and possibilities of improvements are great!

Consequently, if you want to go further please refer to reference books and literature:

- Master teaching book on statistical physics for background (Boltzmann equation, Chapman-Enskog expansion ...)
Ngô C. & Ngô H. “Physique Statistique Introduction”. Dunod, 2008 (in French ☹)
- *Succi S. “The Lattice Boltzmann Equation for Fluid Dynamics and Beyond”. Oxford University Press, 2001, for the Lattice Boltzmann method.*
- Many articles in the fields of physics and numerical methods in fluids.

- Description of the solid phase at the particle scale
- Description of the fluid dynamic in the inter-particle space

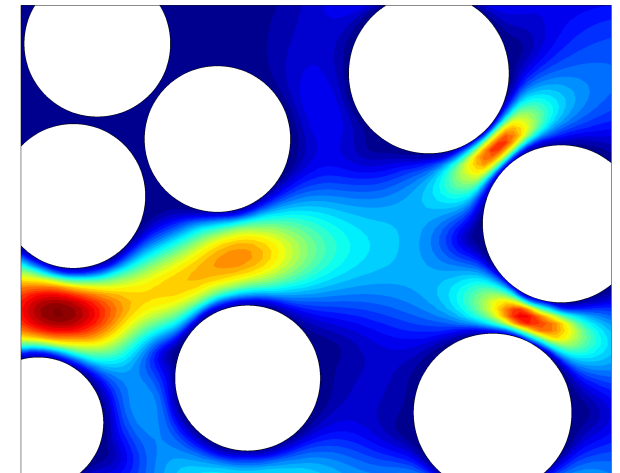
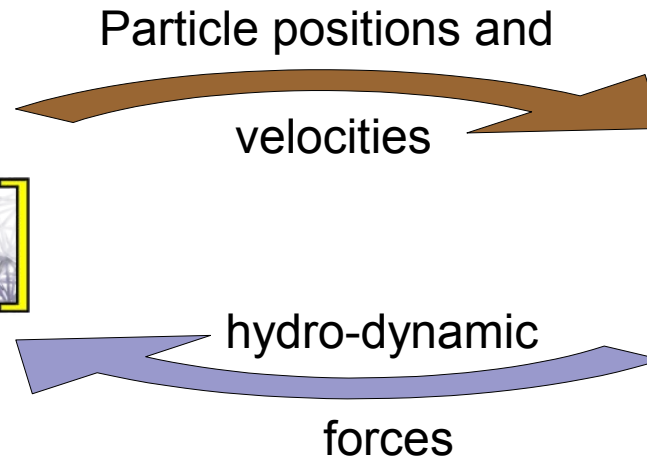
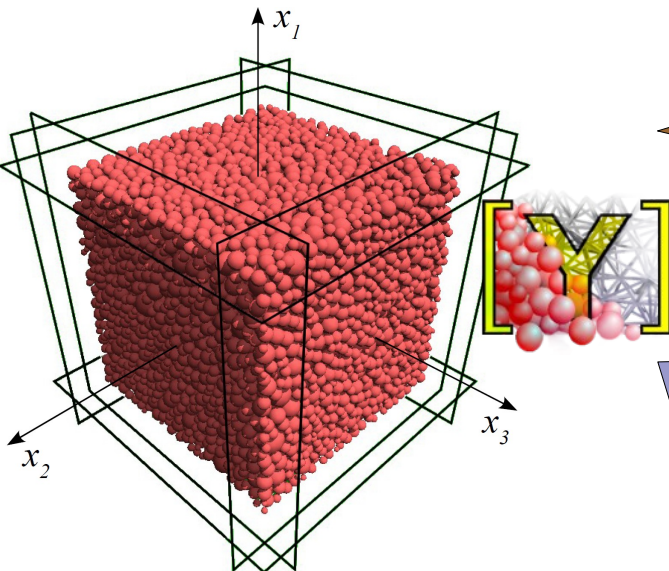


Solid phase: Discrete Element Method
DEM, *Yade Software*

Fluid phase
Lattice Boltzmann Method (LBM)

- Contact stiffnesses
- Contact friction angle
- Contact adhesion

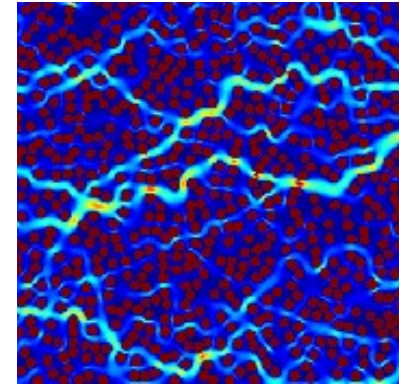
- Fluid viscosity
- position of each solid particle explicitly described



No assumption on fluid/solid interactions: permeability, drag forces, etc... result from the coupling.

LBM, why?

- Description quite easy of moving boundaries with complicated geometrical shape 👍
- Nice numerical implementation (iterative process as for the DEM) 👍
- Versatile method for future development (surface tension and multiphase flows, thermal flow, reactive flow ...) 👍
- Need of a fine lattice (many nodes) to describe interstitial fluid flow 👎
(a minimum of about 10 lattice nodes in a particle diameter seems to be required, but possibility of parallelization)
- Indirect description of the pressure field (related to fluid density), consequently only low pressure variations can be simulated 👎
- Space discretization (lattice) depends on velocity of the fluid flow 👎



⇒ **DEM-LBM coupled method should be applied on a small domain (REV ...)**
⇒ **Should be use essentially to improve the qualitative understanding of physical phenomenon (quantitative approach seems tricky).**

- I. Introduction (what? why?)
- II. Lattice Boltzmann Method (very few words about background)
- III. Practical use of the LBM (main steps to be considered)
- IV. DEM-LBM coupling (exchange of information and time step)
- V. Application to piping erosion.

II. Lattice Boltzmann Method

II-1 Boltzmann equation

Established by Ludwig Boltzmann (1872):

- The Boltzmann Equation aims initially to describe the statistical distribution of one particle (or molecule) in rarefied gas.
- This equation is the cornerstone of the kinetic theory (branch of the statistical physics) dealing with the dynamics of non-equilibrium processes and their relaxation to thermodynamic equilibrium.

Ex: heat up a pan of water, stop the heating: water temperature decreases with time until reaching the temperature of the outside environment and there is thermal equilibrium.

- Originally developed in the framework of dilute gas systems, this equation is now applied in many physics area: interactions in two phase fluids, electron transport in semiconductors...



⇒ **Central object of kinetic theory and Boltzmann Equation: the probability density or distribution function** $f(\vec{x}, \vec{p}, t)$.

$f(\vec{x}, \vec{p}, t)$ is the probability of finding a molecule (or particle) around position \vec{x} at time t with momentum \vec{p} (with $\vec{p} = m\vec{v}$).

The Boltzmann Equation is a non-linear integro-differential equation:

$$\underbrace{\frac{\partial f}{\partial t} + \vec{v} \cdot \frac{\partial f}{\partial \vec{x}} + \frac{\vec{F}^{ext}}{m} \cdot \frac{\partial f}{\partial \vec{v}}}_{\equiv \text{Newton single-particle dynamics}} = \underbrace{\iint (f' f'_1 - f f_1) v_{rel} \sigma(\Omega') d\Omega' d\vec{v}_1}_{\text{Collision between particles}}$$

⇒ **Bhatnagar-Gross-Krook simplified collision operator (1954, BGK operator); can be seen as a “linearised” collision operator:**

$$f(\vec{x}, t) - \frac{1}{\tau} [f(\vec{x}, t) - f^{eq}(\vec{x}, t)]$$

$f^{eq}(\vec{x}, t)$ is an equilibrium distribution function parametrized by macroscopic quantities, density ρ , speed \vec{u} and temperature T .

τ is a typical time-scale associated with relaxation towards the equilibrium distribution function.

II. Lattice Boltzmann Method

II-3 Discretization (LGCA)

⇒ Discretization of space, time, and particle velocities (based on Lattice Gas Cellular Automata (LGCA; Hardy et coll., 1973) ⇒ Lattice Boltzmann Equation:

$$\underbrace{f_i(\vec{x} + \vec{e}_i dt, t + dt)}_{\text{Propagation}} = \underbrace{f_i(\vec{x}, t) - \frac{1}{\tau} [f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t)]}_{\text{Collision}}$$

i represents a discrete space direction.

\vec{e}_i is a discrete velocity of propagation in direction i
of the distribution function f_i

⇒ At each node of the lattice (the discretized space) macroscopic properties are deduced from:

density:

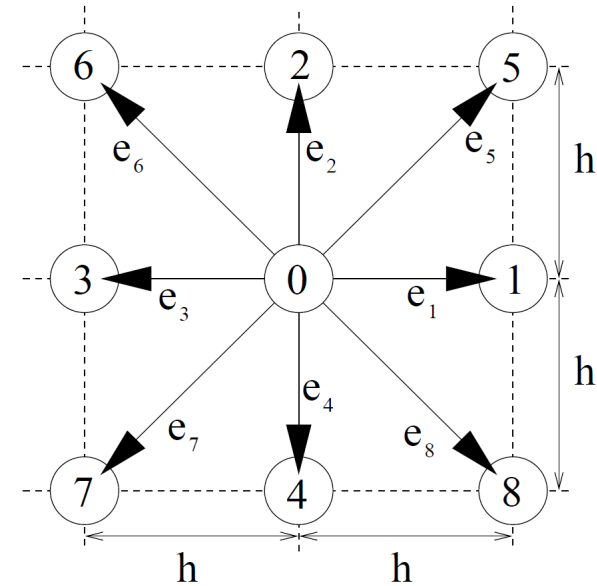
$$\rho = \sum_{i=0}^8 f_i$$

velocity :

$$\vec{v} = \frac{1}{\rho} \sum_{i=0}^8 f_i \vec{e}_i$$

pressure: $p = C_s^2 \rho$ with $C_s = C/\sqrt{3}$ where C is the lattice speed $C = h/dt$

D2Q9 model



⇒ Derivation of incompressible Navier-Stokes Equations based on the Chapman-Enskog Expansion:

- This procedure is based on a double Taylor series expansion from a spatial and temporal point of view, involving a multi-scale representation of space and time variables.

- Conservation of momentum, mass and energy at macroscopic scale are found for:

- a small Mach number $M = \frac{v_{max}}{C}$

- small density variations (in classical LBM the fluid is slightly compressible)

- an equilibrium distribution function writing:

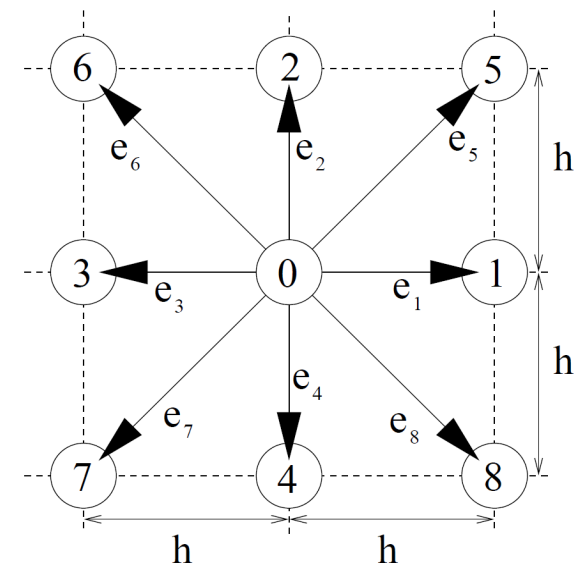
$$f_i^{eq} = w_i \rho \left(1 + \frac{3}{C^2} \vec{e}_i \cdot \vec{v} + \frac{9}{2C^4} (\vec{e}_i \cdot \vec{v})^2 - \frac{3}{2C^2} \vec{v} \cdot \vec{v} \right)$$

with $w_0 = 4/9$; $w_{1,2,3,4} = 1/9$ and $w_{5,6,7,8} = 1/36$ for the D2Q9 model.

- Identification of the relation between τ and the kinematic viscosity ν :

$$\nu = \frac{1}{3} \left(\tau - \frac{1}{2} \right) Ch \quad (\tau > 0.5 \text{ for } \nu > 0)$$

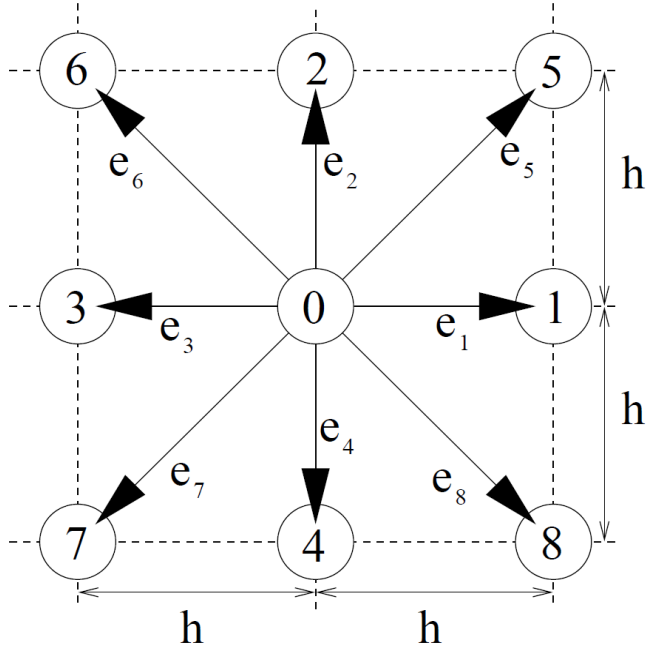
D2Q9 model



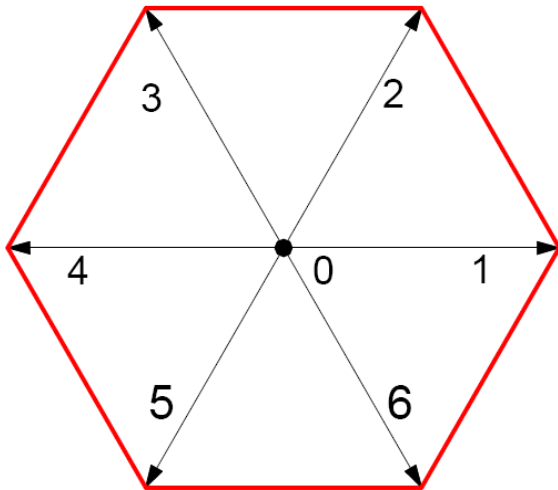
III. Practical use of the LBM

III-1 Space discretization model

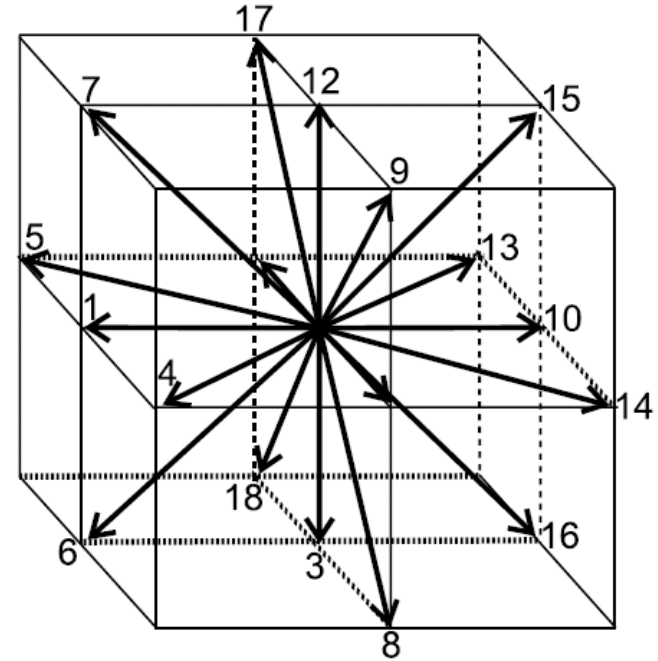
D2Q9 model



D2Q7 model



D3Q19 model (Mansouri et al., 2009)



D3Q15

D3Q27

...

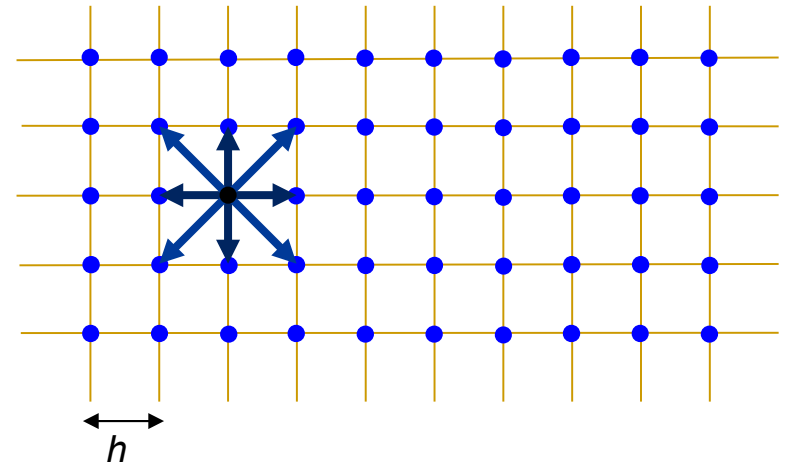
Some space discretization models are unable to recover Navier-Stokes!

III. Practical use of the LBM

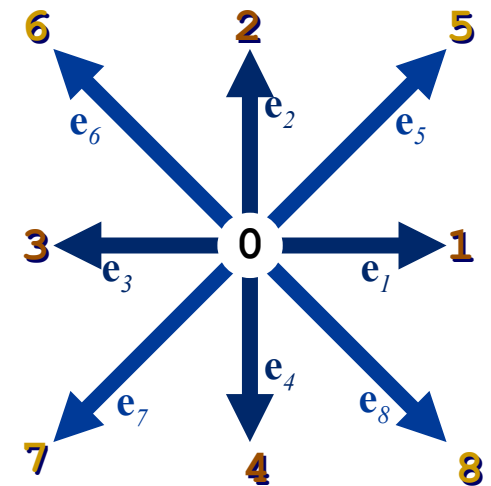
III-1 Space discretization model

D2Q9 model

- fixed lattice : h
 - time step : dt
- } $C = h/dt$
- for each node, we define:
 - 9 directions: i
 - 9 discrete velocities: \vec{e}_i
 - 9 distribution functions: f_i



$$\vec{e}_i = \begin{cases} (0, 0) & \text{if } i = 0 \\ C \left(\cos \left(\frac{\pi(i-1)}{2} \right), \sin \left(\frac{\pi(i-1)}{2} \right) \right) & \text{for } i = 1, \dots, 4 \\ C \left(\cos \left(\frac{\pi(2i-9)}{4} \right), \sin \left(\frac{\pi(2i-9)}{4} \right) \right) & \text{for } i = 5, \dots, 8 \end{cases}$$



III. Practical use of the LBM

III-1 Space discretization model

D2Q9 model

- fixed lattice : h
 - time step : dt
- } $C = h/dt$
- for each node, we define:
 - 9 directions: i
 - 9 discrete velocities: \vec{e}_i
 - 9 distribution functions: f_i
 - macroscopic properties:

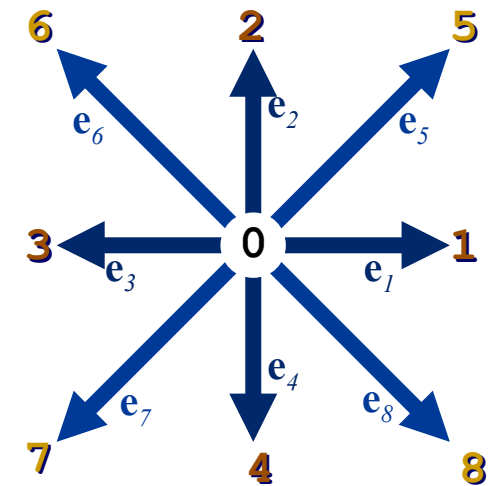
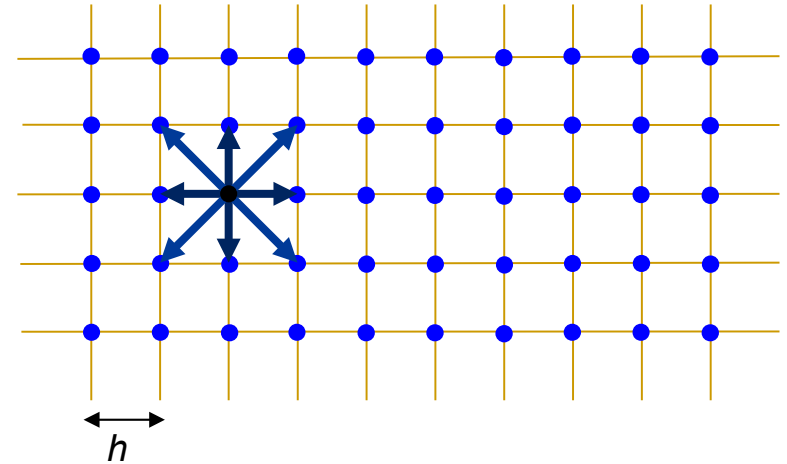
density:

$$\rho = \sum_{i=0}^8 f_i$$

velocity :

$$\vec{v} = \frac{1}{\rho} \sum_{i=0}^8 f_i \vec{e}_i$$

pressure: $p = C_s^2 \rho$ with $C_s = C/\sqrt{3}$



III. Practical use of the LBM

III-2 A two steps iterative process

LB method in 2 steps: collisions and propagation

- consider 3 distributions functions arriving on a node

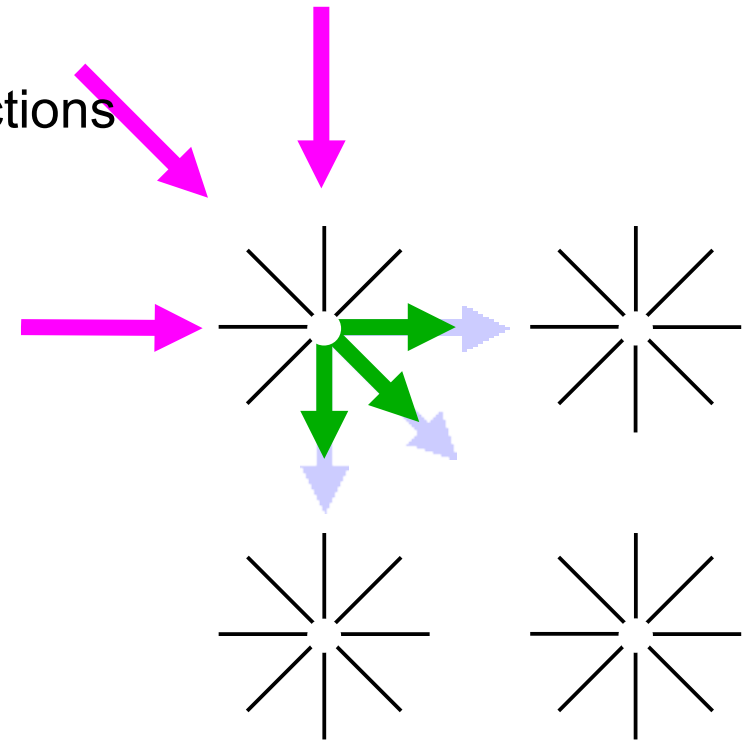
- **collisions:** relaxation towards equilibrium functions

$$f_i(\vec{x}, t^+) = f_i(\vec{x}, t) - \frac{1}{\tau} [f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t)]$$

$$\left\{ \begin{array}{l} f_i^{eq} = w_i \rho \left(1 + \frac{3}{C^2} \vec{e}_i \cdot \vec{v} + \frac{9}{2C^4} (\vec{e}_i \cdot \vec{v})^2 - \frac{3}{2C^2} \vec{v} \cdot \vec{v} \right) \\ (i = 1, \dots, 8) \quad \Delta t = \left(\tau - \frac{1}{2} \right) \frac{h^2}{3\nu} \end{array} \right.$$

- propagation along each direction

$$f_i(\vec{x} + \vec{e}_i dt, t + dt) = f_i(\vec{x}, t^+)$$



III. Practical use of the LBM

III-2 A two steps iterative process

LB method in 2 steps: collisions and propagation

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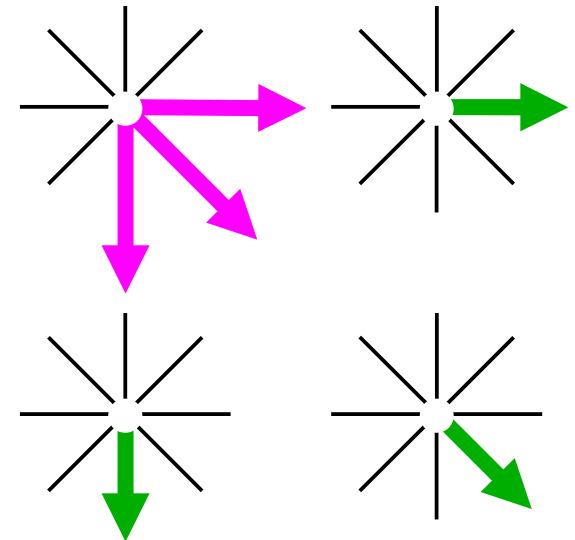
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- **propagation** along each direction

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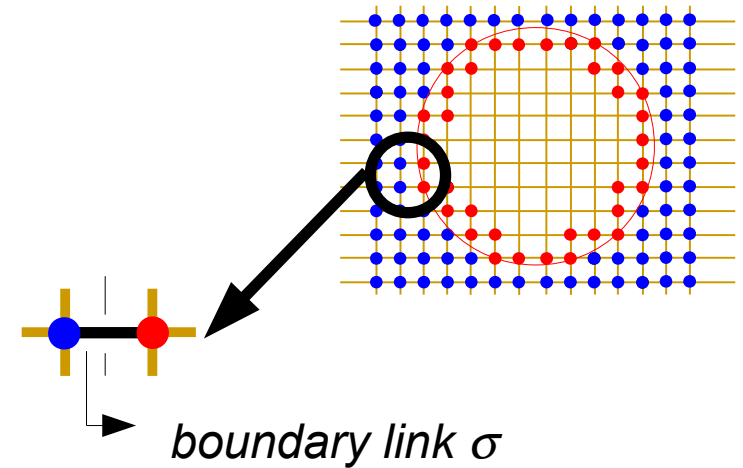


III. Practical use of the LBM

III-3 No slip condition on solid obstacle boundary

- discretize the obstacles
- differentiate « fluid » nodes and « solid » nodes
- bounce back on each boundary link:

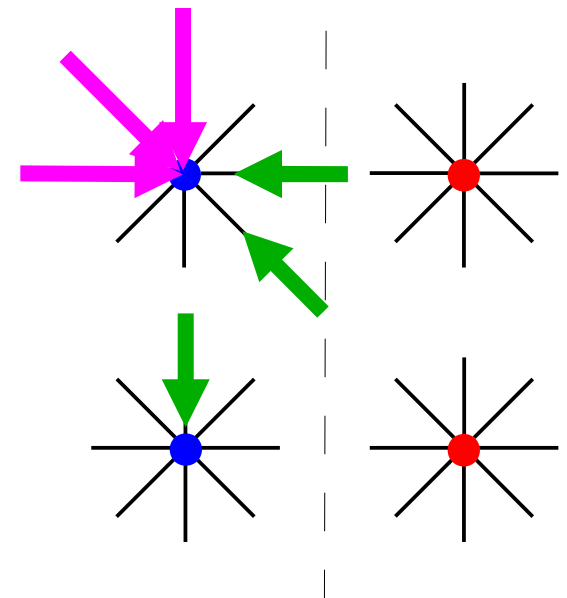
$$f_{-\sigma i}(\vec{x}_{FB}, t + dt) = f_{\sigma i}(\vec{x}_{FB}, t^+)$$



Obstacle boundary, $V_b = 0$

⇒ Vanishing of the macroscopic fluid velocity at the point where distribution functions are reflected.

⇒ For the LBM, the solid boundary is halfway between solid and fluid nodes.



III. Practical use of the LBM

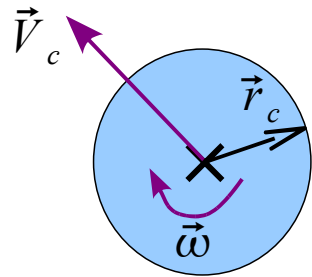
III-3 No slip condition on solid obstacle boundary

Case of moving solid obstacles:

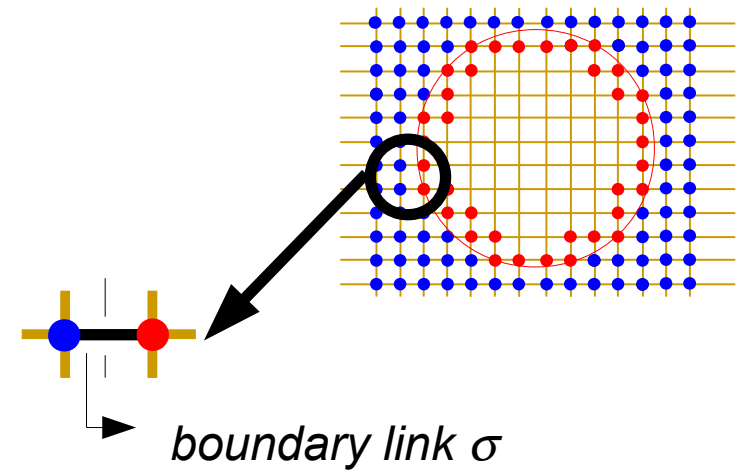
$$f_{-\sigma i}(\vec{x}_{FB}, t + dt) = f_{\sigma i}(\vec{x}_{FB}, t^+) - 2\alpha_i \vec{V}_b \cdot \vec{e}_i$$

$$\alpha_i = 3w_i \rho C^2$$

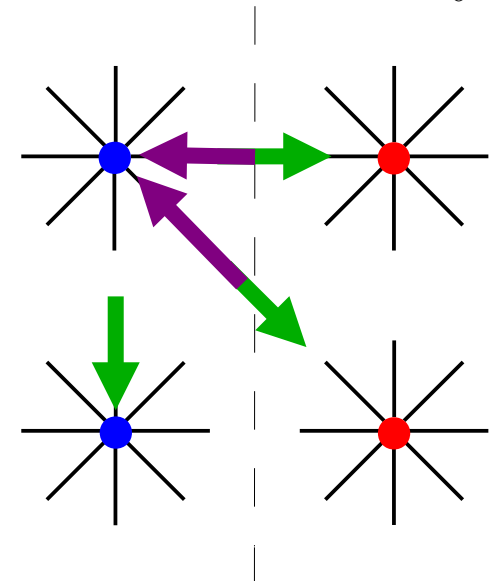
\vec{V}_b is the solid velocity at the middle of the boundary link, for a circular solid particle:



$$\vec{V}_b = \vec{V}_c + \vec{\omega} \wedge \vec{r}_c$$



Obstacle boundary, $V_b \neq 0$



III. Practical use of the LBM

III-3 No slip condition on solid obstacle boundary

Force applied by fluid on solid obstacles:

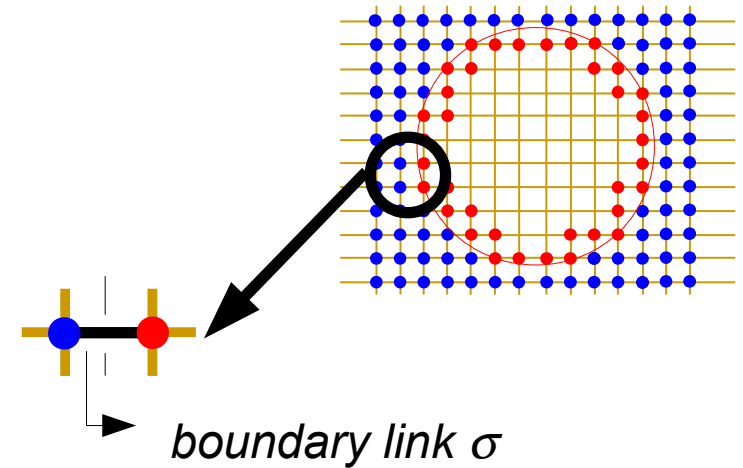
- Force (and then torque) is obtained by derivation of the momentum exchange with respect to time:

$$\vec{F}_\sigma(\vec{x}, t + \frac{1}{2}dt) = 2\frac{\Omega}{dt} \left[f_{\sigma i}(\vec{x}, t^+) - \alpha_i \vec{V}_b \cdot \vec{e}_i \right] \vec{e}_{\sigma i}$$

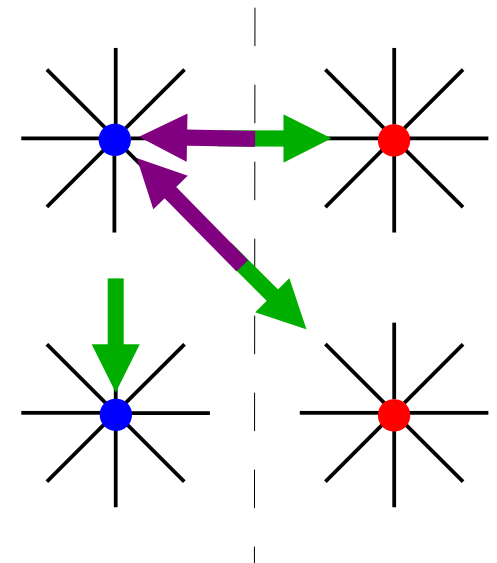
$$\vec{T}_\sigma(\vec{x}, t + \frac{1}{2}dt) = \vec{r}_c \times \vec{F}_\sigma(\vec{x}, t + \frac{1}{2}dt)$$

- For the whole solid boundary:

$$\vec{F}_h(t + \frac{1}{2}dt) = \sum_{\sigma} \vec{F}_\sigma(\vec{x}, t + \frac{1}{2}dt)$$



Obstacle boundary, $V_b \neq 0$



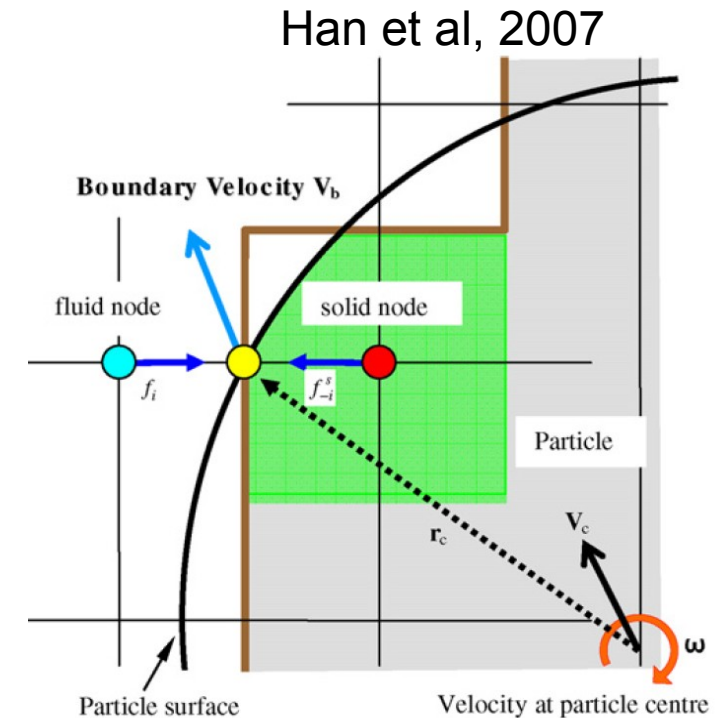
III. Practical use of the LBM

III-3 No slip condition on solid obstacle boundary

⇒ The bounce back rule presented here is one of the simplest (and rough) way to deal with interactions between fluid and moving solid boundaries.

⇒ More complex scheme exist such as the immerse boundary scheme where the LB equation is weighted by the solid/fluid surface ratio at the vicinity of the node considered.

⇒ The classical bounce back rule limit the computation cost and is satisfactory as a first approximation.



III. Practical use of the LBM

III-4 Pressure boundary condition

The distribution function $f_i(\vec{x}, t)$ is the only object handled with the LBM.

⇒ **Pressure and velocity boundary conditions cannot be imposed directly.**

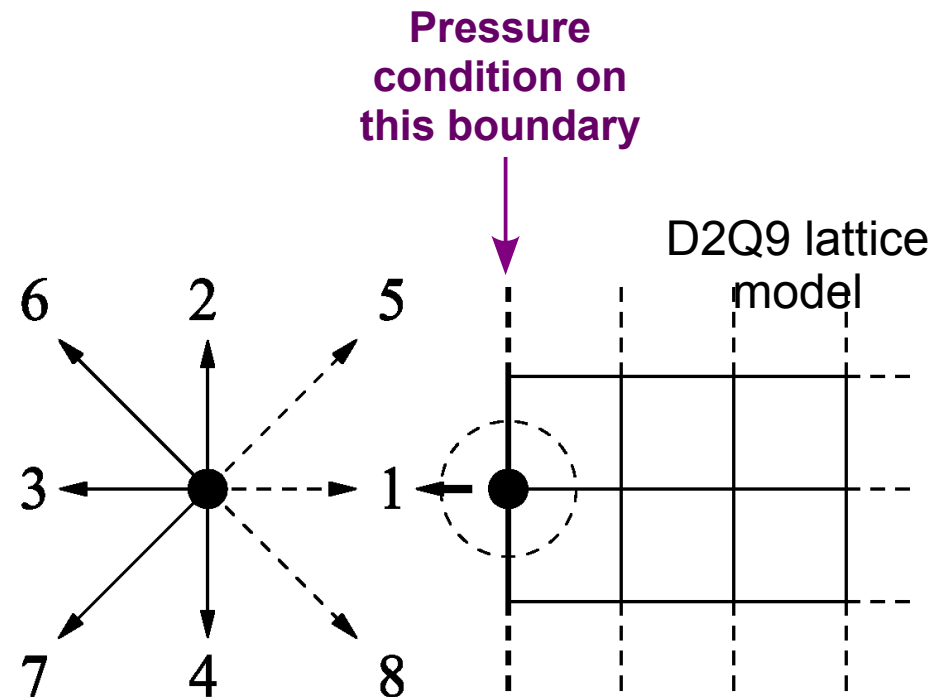
⇒ **Distribution functions have to be defined to match the desired boundary condition (see work of Zou & He, 1997; Succi 2001).**

Case of a pressure limit condition

For the considered node and after the propagation step:

- $f_{2,3,4,6,7}$ are known,
- $f_{1,5,8}$ are unknown.

⇒ **Need of three equations where unknown distribution functions are expressed with respect to the macroscopic pressure and velocity.**



III. Practical use of the LBM

III-4 Pressure boundary condition

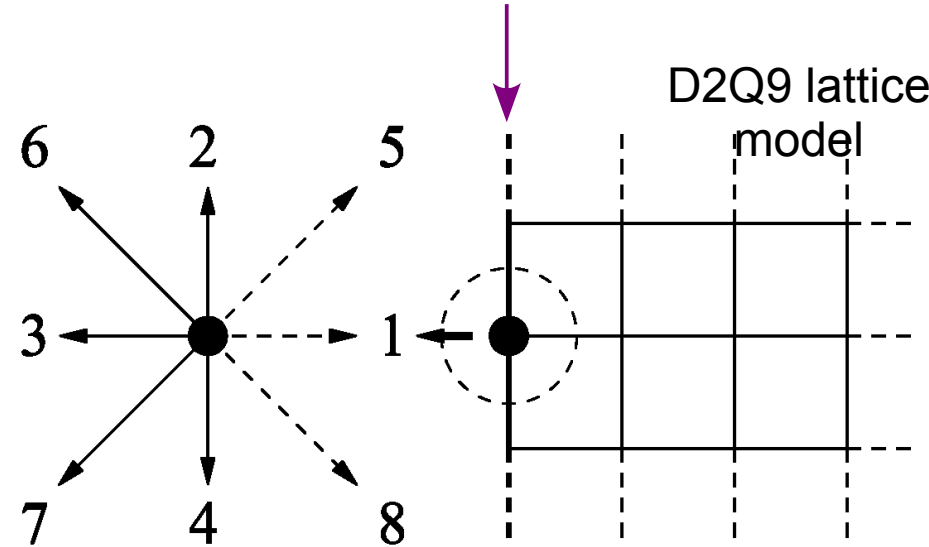
$$\vec{v} = \frac{1}{\rho} \sum_{i=0}^8 f_i \vec{e}_i$$

Projection on the two
space directions

$$\begin{cases} \bar{f}_1 + \bar{f}_5 + \bar{f}_8 = \bar{\rho} \bar{v}_x + \bar{f}_3 + \bar{f}_6 + \bar{f}_7 \\ \bar{f}_5 - \bar{f}_8 = \bar{\rho} \bar{v}_y + (-\bar{f}_2 + \bar{f}_4 - \bar{f}_6 + \bar{f}_7) \end{cases}$$

$$\rho = \sum_{i=0}^8 f_i$$

$$\bar{f}_1 + \bar{f}_5 + \bar{f}_8 = \bar{\rho} - (\bar{f}_0 + \bar{f}_2 + \bar{f}_3 + \bar{f}_4 + \bar{f}_6 + \bar{f}_7)$$



III. Practical use of the LBM

III-4 Pressure boundary condition

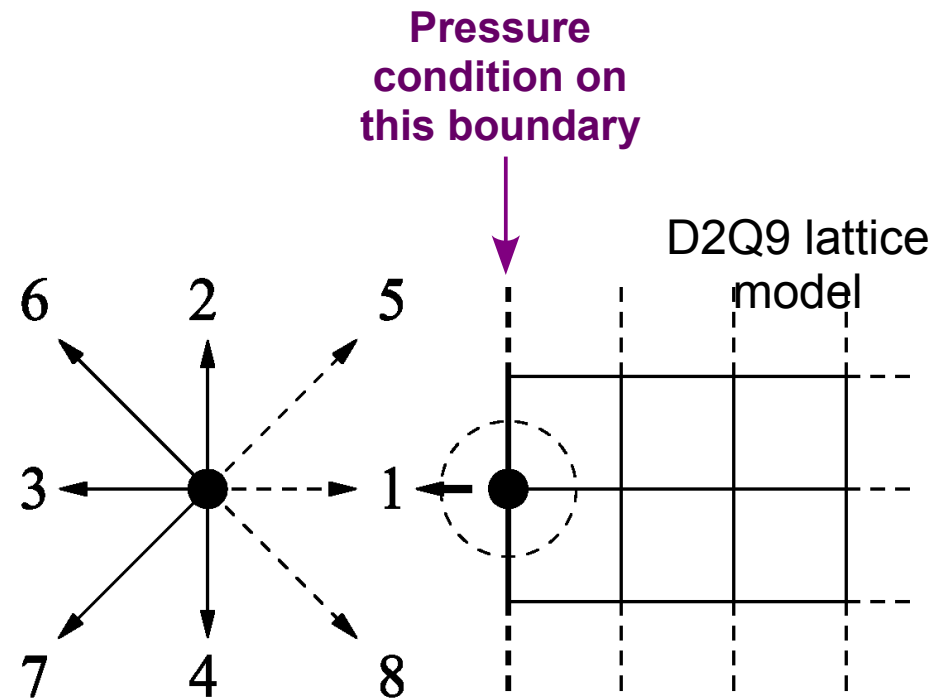
$\Rightarrow \rho? \quad v_x? \quad v_y?$

- Pressure condition \equiv density condition $p = C_s^2 \rho$
- Assumption: tangential velocity to the boundary is nil, $v_y = 0$
- Additional equation: bounce back rule for the non-equilibrium part of the distribution functions normal to the boundary (Zou & He, 1997).

$$f_1 - f_1^{eq} = f_3 - f_3^{eq}$$

By developing the equilibrium functions

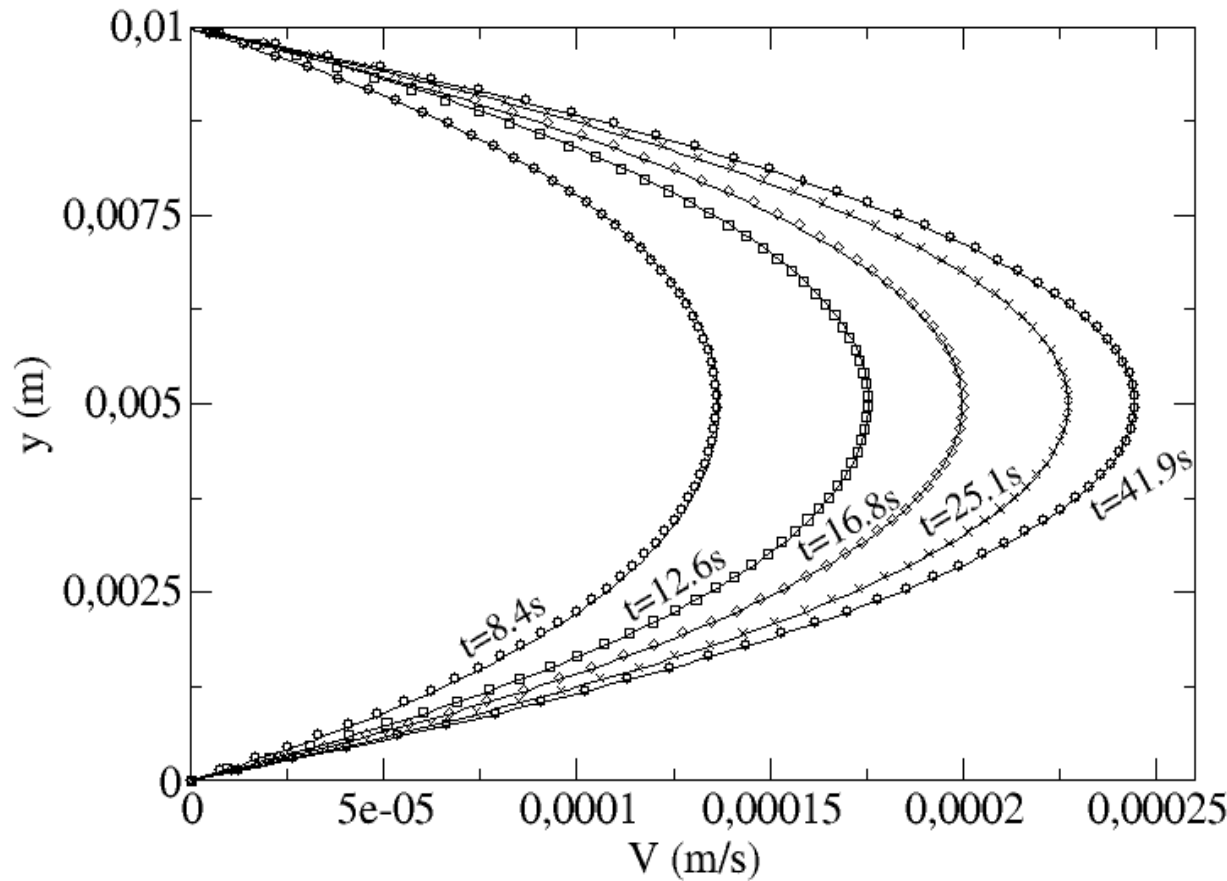
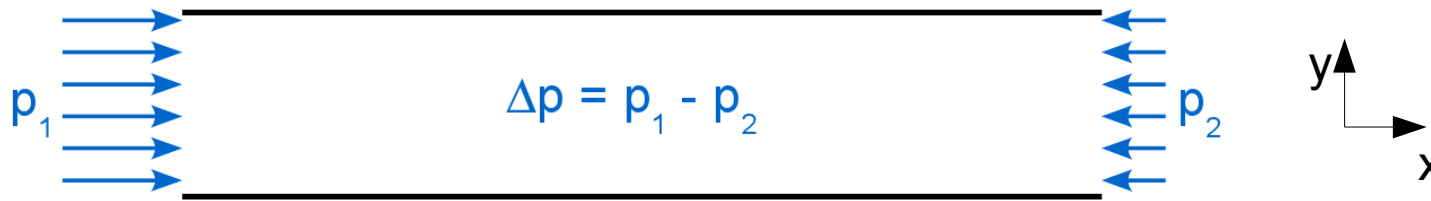
$$\bar{f}_1 = \bar{f}_3 + \frac{2}{3} \bar{\rho} \bar{v}_x$$



III. Practical use of the LBM

III-5 Validation on simple flow cases

Poiseuille flow

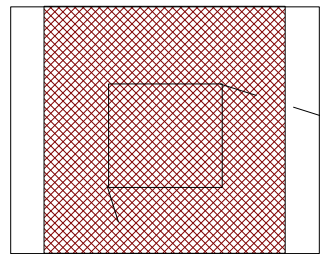


⇒ agreement with serie solutions for transient and stationnary solutions

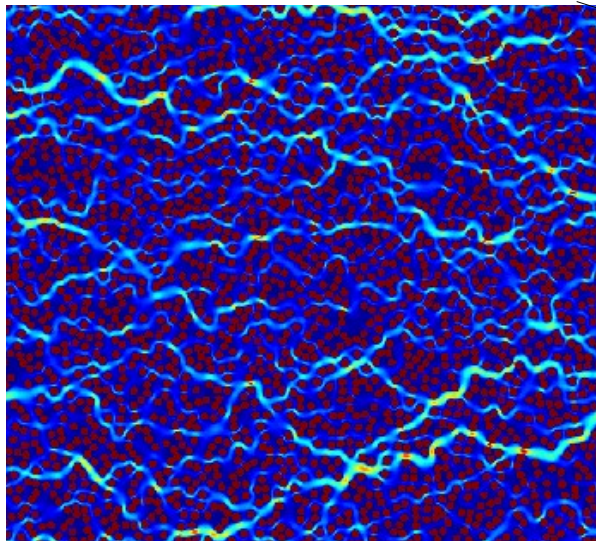
(Lominé et al, AGS'10, 2010)

Fluid flow in porous media

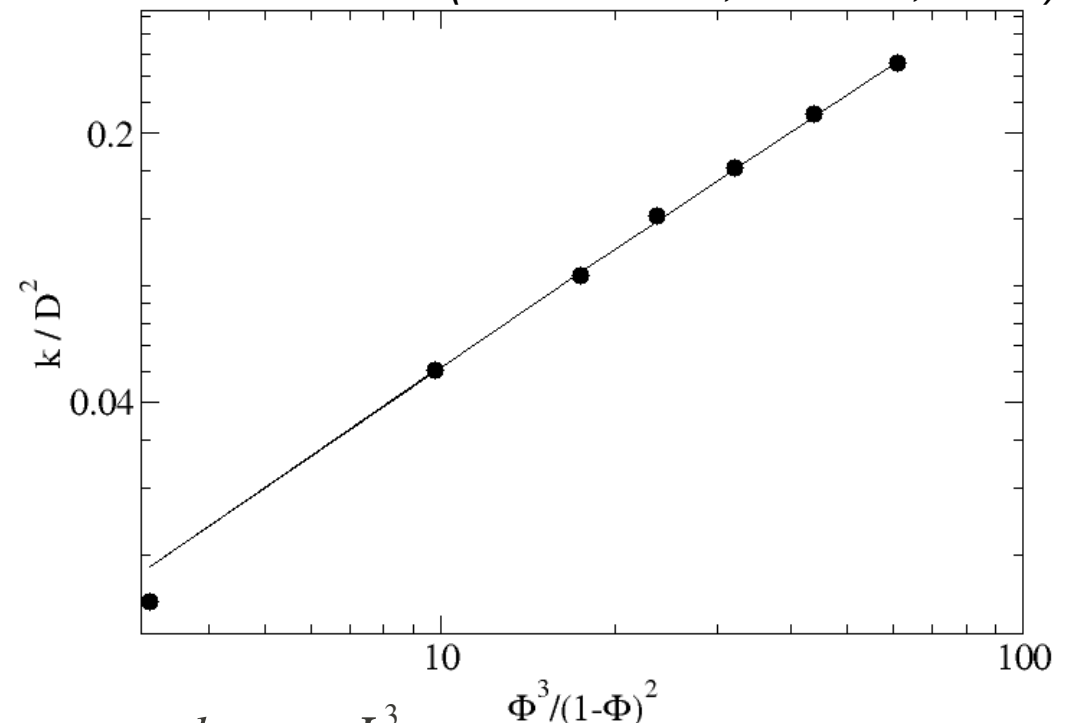
We consider bi-dimensional porous media with porosity Φ , made with spherical particles of diameter D .



D (Φ) vary and N vary from ~ 3000 to ~ 5000 particles



(Lominé et al, AGS'10, 2010)



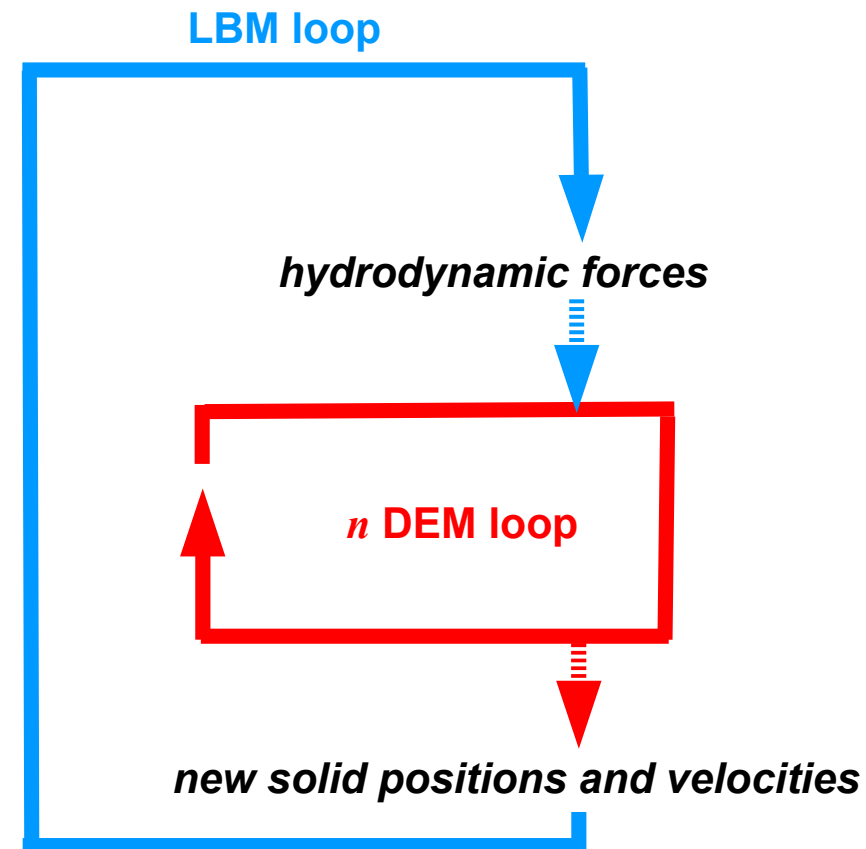
\Rightarrow we retrieve the Kozeny-Carman relation: $\frac{k}{D^2} \propto \frac{\Phi^3}{(1-\Phi)^2}$

- DEM time step is limited for stability condition by a critical time step: $dt_{DE} < dt_{DE}^{cr} = 2\pi\sqrt{m/k}$
- LBM time step given by: $dt = \frac{1}{3\nu} \left(\tau - \frac{1}{2} \right) h^2$

⇒ For usual material parameters (contact stiffness, solid density, fluid density and viscosity): **DEM time step < LBM time step.**

⇒ The DEM loop is considered as a subcycle of the LBM loop (Feng et al., 2007)

- The DEM time step is adjusted such as an integer number n of DEM loop can be performed in one LBM loop: $dt = n dt_{DE}$
- Same value of F_h applied on solid particles during the n DEM loop
(*smooth solid particle motion required during the n DEM loop*)

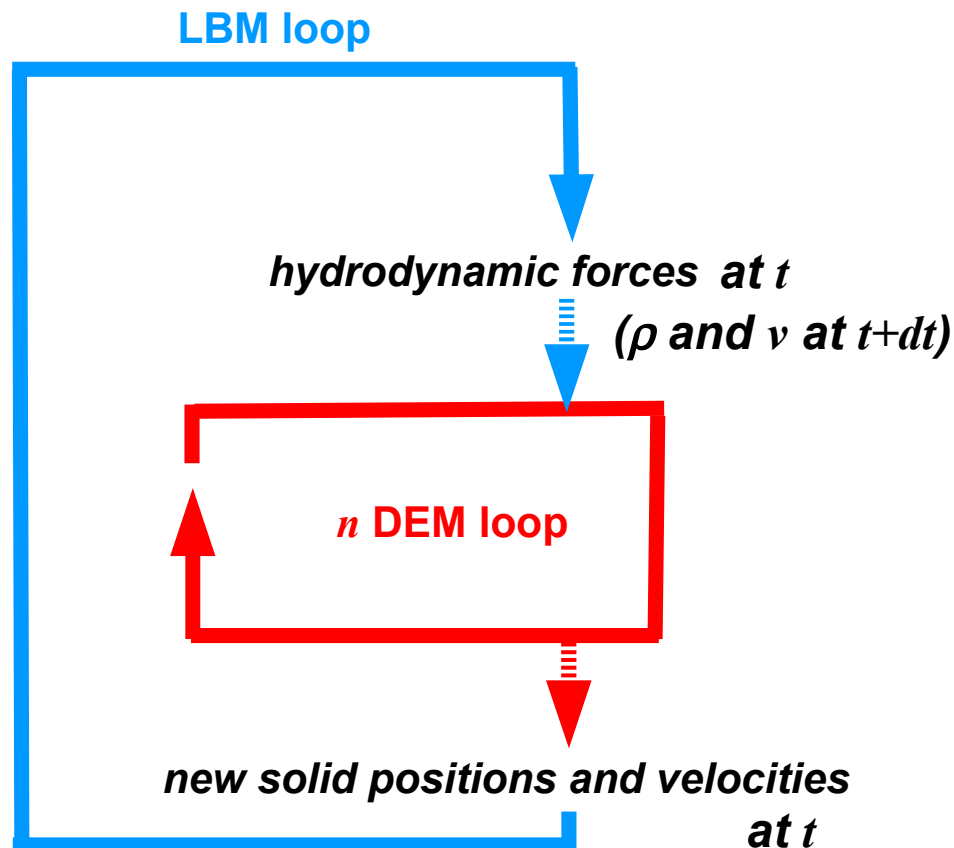


IV. DEM-LBM coupling

IV-2 Hydrodynamic forces and Newton's law

Action of fluid on solid particles is simply taken into account in Newton's law:

$$\begin{array}{ccc} \text{Contacts (DE method)} & \begin{array}{l} m \vec{y} = \vec{F}_c + \vec{F}_h \\ J \vec{\omega} = \vec{T}_c + \vec{T}_h \end{array} & \text{Fluid (LB method)} \end{array}$$



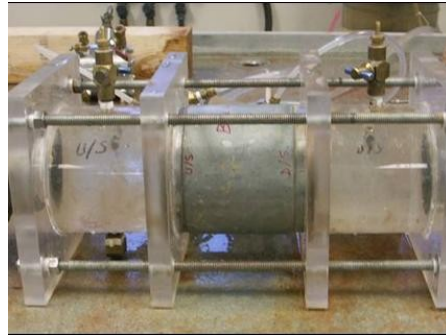
V. Application to piping erosion

V-1 Characterization of soil erodability

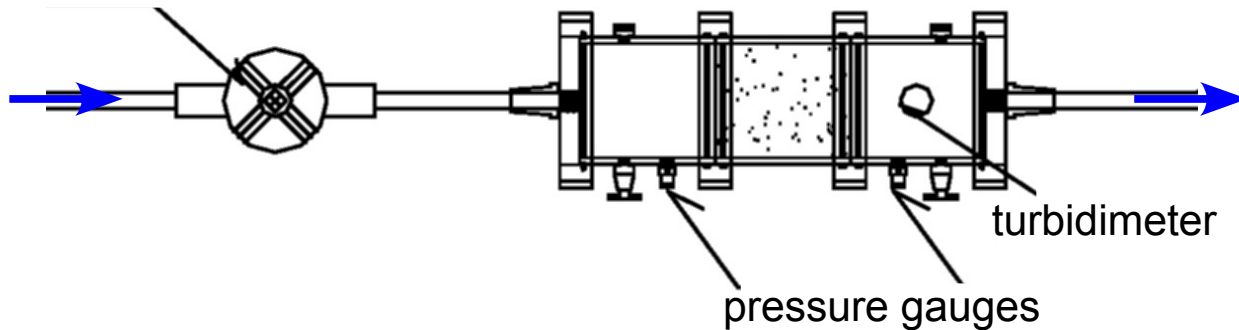
- Laboratory test: Hole Erosion Test (HET)

(Regazzoni, 2009)

(Pham, 2008)

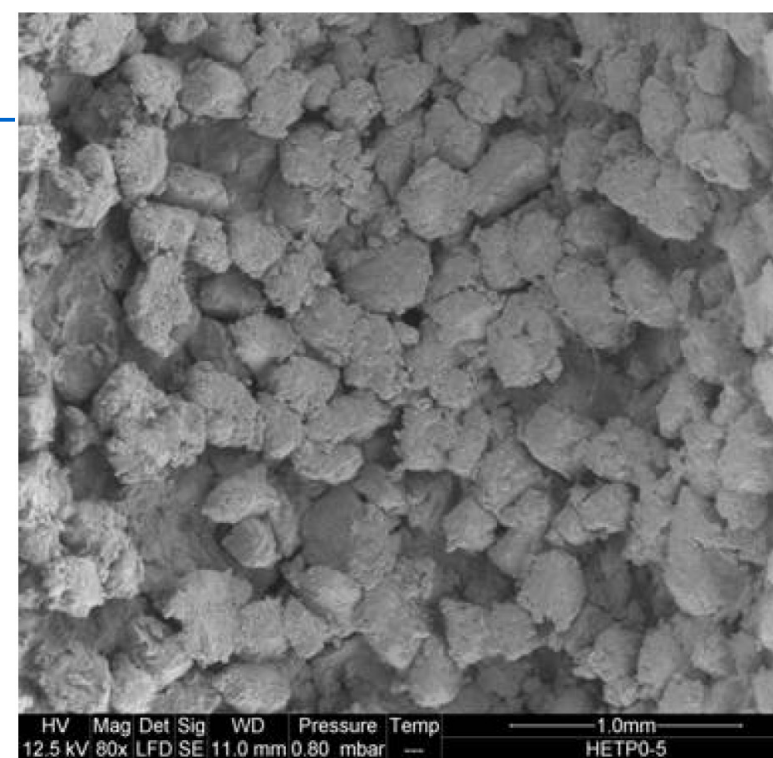


Flowmeter

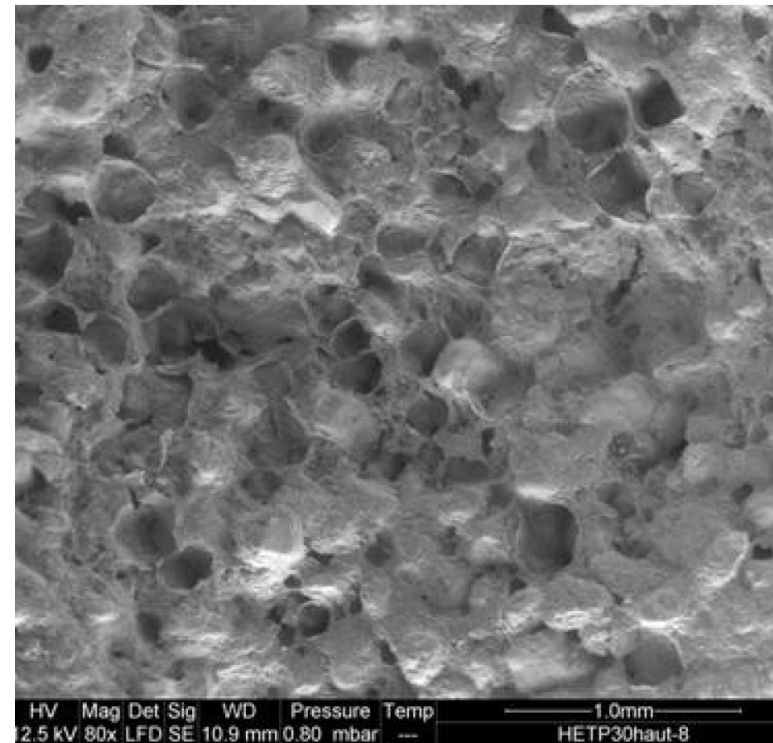


- Characterisation of particle detachments under hydro-mechanical loadings

- Description of mechanisms involved at microscopic scale.
- Identification of relevant parameters related to the solid and fluid phase



(Pham, 2008: sand and clay mix)



V. Application to piping erosion

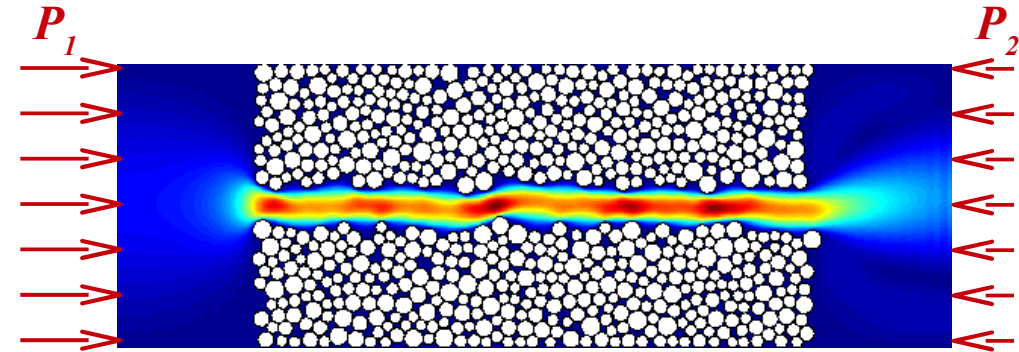
V-2 Model description

⇒ Simplified 2D Hole Erosion Test (HET):

- Cohesive frictional granular assembly:

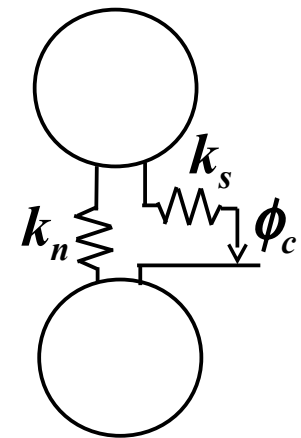
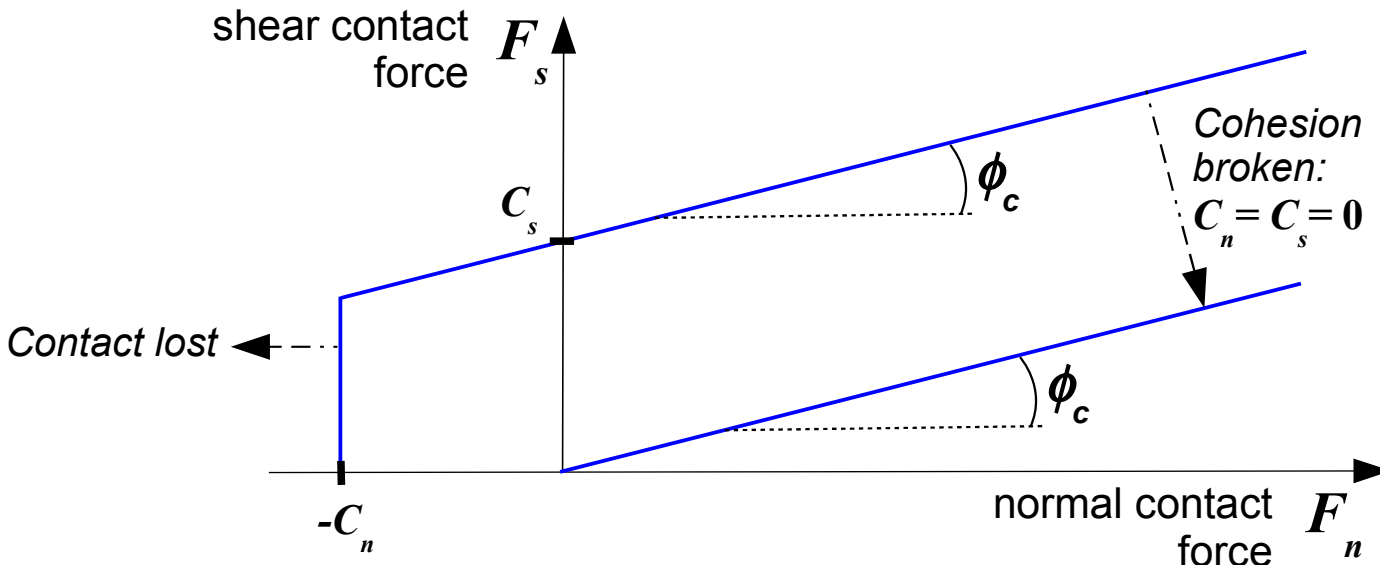
$$\phi_c = 20^\circ \quad C = -C_n = C_s$$

- Initial hole drilled in the granular assembly,
- Water flow under constant pressure gradient: $\Delta P = P_1 - P_2$.



800 solid particles; fluid lattice of 335 000 nodes

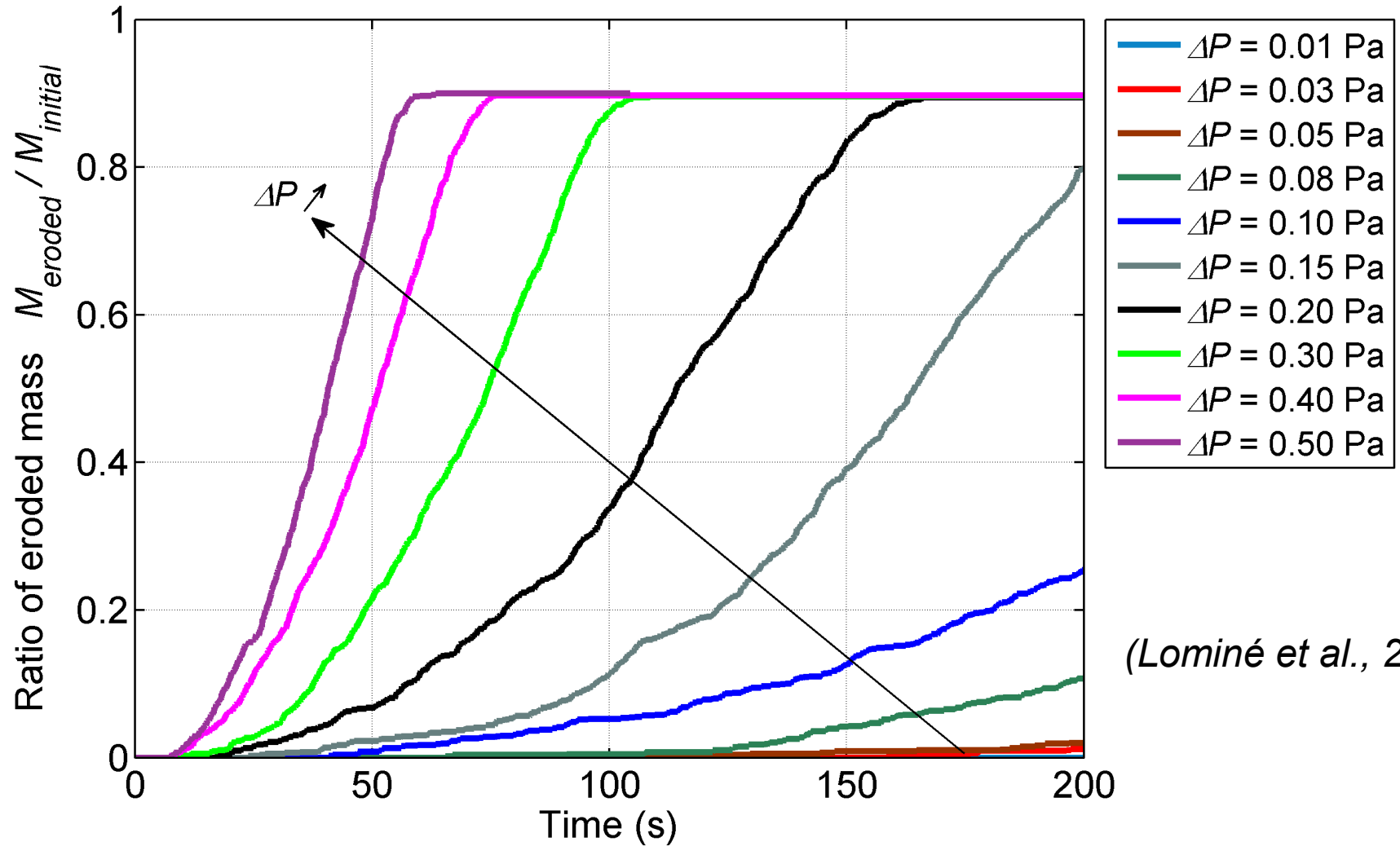
⇒ Brittle cohesive inter-particle contacts:



V. Application to piping erosion

V-3 Numerical results

⇒ Ratio of eroded mass for a cohesion $C/d = 0.506 \text{ N/m}$



(Lominé et al., 2011)

→ No erosion for $\Delta P = 0.01 \text{ Pa}$.

→ Acceleration of kinetic of erosion when ΔP increases.

V. Application to piping erosion

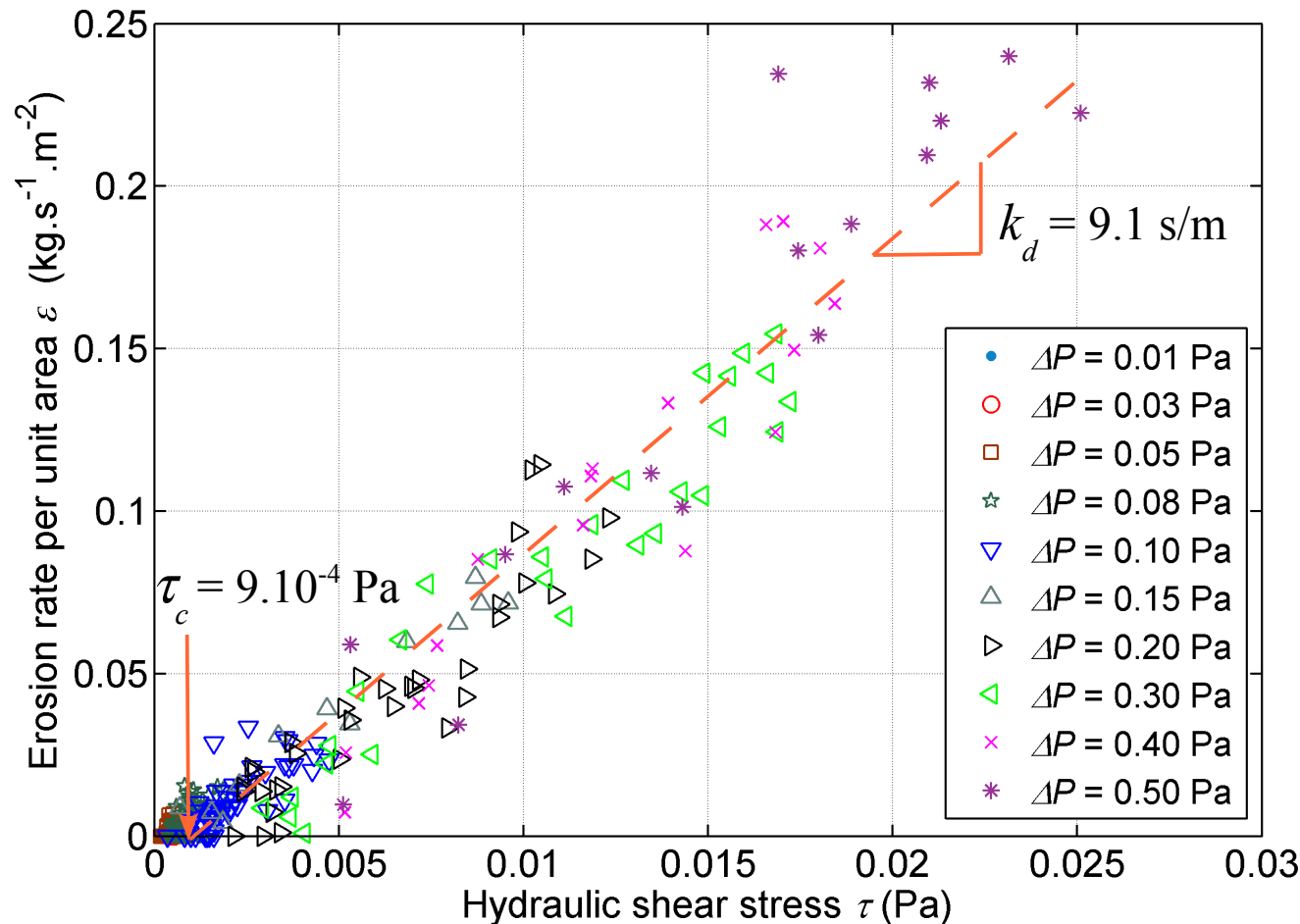
V-3 Numerical results

⇒ Classical interpretation with respect to the hydraulic shear stress τ :

$$\dot{\epsilon} = k_d (\tau - \tau_c) \text{ if } \tau > \tau_c \quad (\text{Shields 1936, Wan \& Fell 2002})$$

τ_c : critical shear stress

k_d : erosion rate .



→ Hydraulic shear stress computed along the hole border:

$$\tau = \nu \rho_0 \frac{dV_x}{dy}$$

(Lominé et al., 2011)